

Solid Oxide Fuel Cell Cathode Enhancement Via Single-step Infiltration

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Outline

- **About Materials & Systems Research Inc. (MSRI)**
- **R&D Motivation**
- **Accomplishments**
- **Results and Discussions**
- **Summary and Future Work**

Materials & Systems Research Inc.

MSRI specializes in materials and electrochemical engineering for power generation and energy storage applications: fuel cells/electrolyzers, storage batteries, and thermoelectric converters.

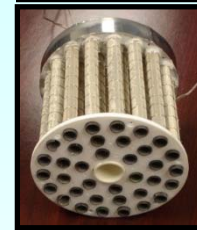
MSRI has 12 employees: 5 with PhDs in material, mechanical, chemical, & chemistry

Fuel Cell/Electrolyzer

- Start from off-the-shelf powders
- Both planar and tubular cells
- Per-cell active area varying from 1 to 400 cm²
- Stacks/bundles from 10 W to 4 kW

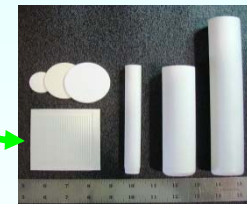


MSRI's
Technology
processing
&
solutions



Sodium-beta Battery

- Advanced Na⁺-conducting ceramic electrolyte
- Unique battery designs



Motivation for Cathode Enhancement

- High power density, long-term reliability & minimal degradation are critical to success of SOFC technologies and fast market penetration
 - **cost target:** stack cost < \$225/kWe (cathode material cost ~ 18%, or ~ \$40/kWe)
 - **degradation rate:** 0.2~1% per 1000 hours operation
- **Cathode polarization losses** attribute significant amount to total cell losses
- **Cathode development:** High-performing cathode materials, or/and cathode processing optimization
 - infiltration of a nano-structured/nano-sized catalyst has been proven to be one of most effective/efficient means for cathode enhancement
 - challenges
 - key parameters determining the success of infiltration process, including adaptability to the pre-established cathode backbones, precursor solution concentration, surfactant, wetting agent, evenness of catalyst distribution along cathode backbones
 - simplicity
 - cost-effective
 - scalable for large cells
 - durability (stability) & process repeatability

Objective & Accomplishments

Objective: to develop and implement an advanced cathode deposition process via infiltrating a nano-catalyst(s) into pre-established cathode backbones for SOFC performance enhancement

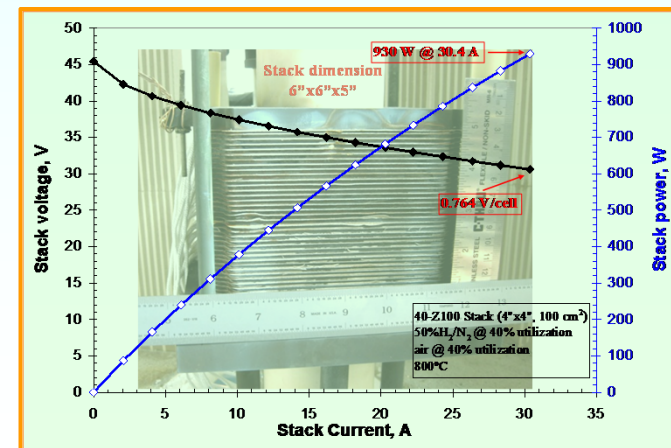
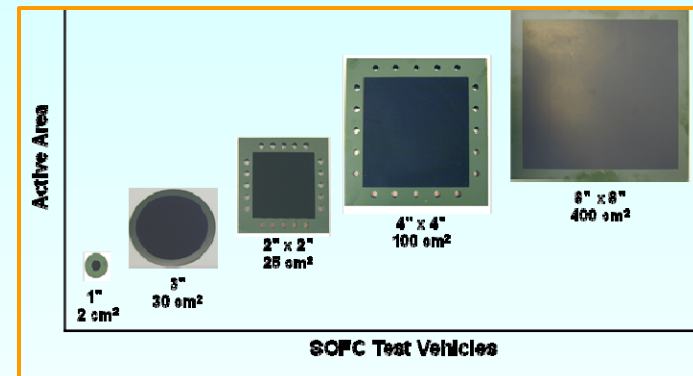
Accomplishments:

- Developed and implemented a single-step VPIT process for infiltrating a nano-sized electrocatalyst into pre-established cathode backbones with per-cell active area varying from 2 cm² to 100 cm²
- Developed a Gen-3 infiltration apparatus for large cell applications
- Investigated electrocatalyst loading profile along the CIL and CCCL of 100 cm² cells after the single-step VPIT process
- Developed a viable strategy to mitigate cell degradation and was validated over accumulated 35,000 cell-hour tests
- Improved single cell performance more than 80% after catalyst infiltration
- Demonstrated single cell (100 cm²) degradation rates ~ 3.5%/1khrs @ 0.5A/cm² (>1100 hrs) and 5%/1khr @ 0.75 A/cm² (>1400hrs, on-going)
- Improved short stacks performance by 40% upon catalyst infiltration, and demonstrate stack degradation rate ~ 3.1%/1khr @ 0.5A/cm²

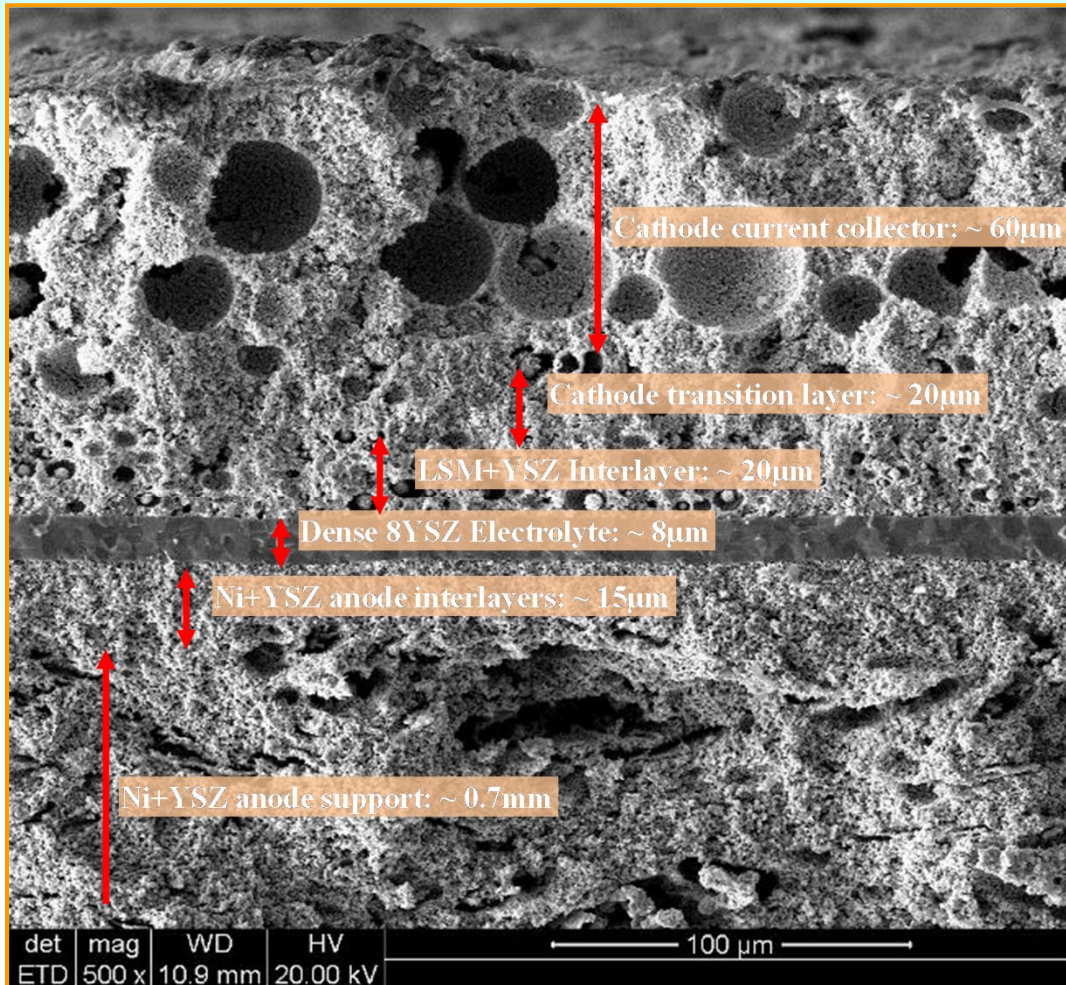
Anode-supported SOFC Fabrication

Baseline cell fabrication for infiltration studies

- MSRI's standard cell fabrication process involves sequential steps: starting from powder mixing/milling → anode tape casting → cell shaping by laser cutting → bisquing → AIL & electrolyte layer application → sintering → CIL/CTL/CCCL deposition by screen-printing & firing.



Cell Construction and Test

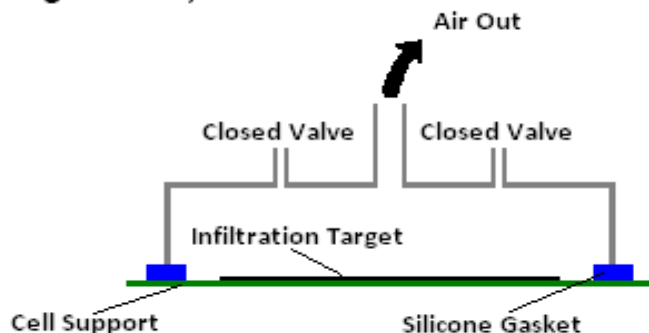


SEM micrograph of a baseline cell

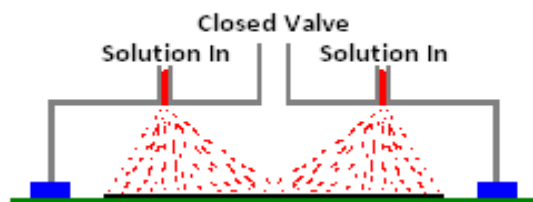
- In this study, all cells were constructed with:
 - Ni-YSZ anode support (~0.7 mm)
 - YSZ-based electrolyte (8 μm)
 - **LSM-based cathode system**, consisting of LSM+YSZ as CIL, LSM+LSCF as CTL, and LSCF as CCCL
- Per-cell active area:
 - Button cell: 2 cm²
 - Single cell: 100 cm²
- Test conditions:
 - Either H₂ or a diluted H₂ as the fuel
 - Low fuel utilization for button cells
 - Controlled utilization for single cells and stacks, typically 40% ~ 80%
 - **Cell temperature** fixed @ 800°C for LSM-based cathode cells and 700°C for LSCF-based cathode cells

Single-step Infiltration Technique

Step 1: Align device, evacuate chamber and electrode pores



Step 2: Deliver specific volume of catalyst solution



Step 3: Apply heat and reintroduce atmospheric pressure

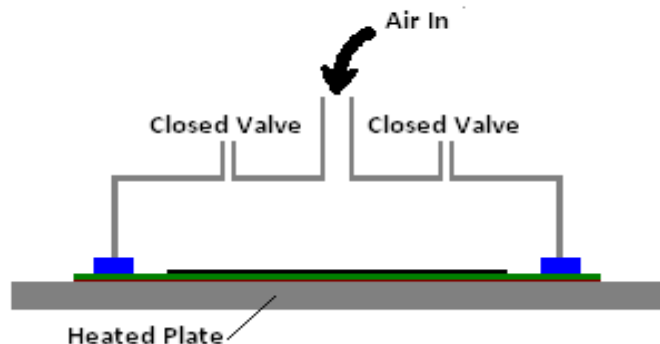
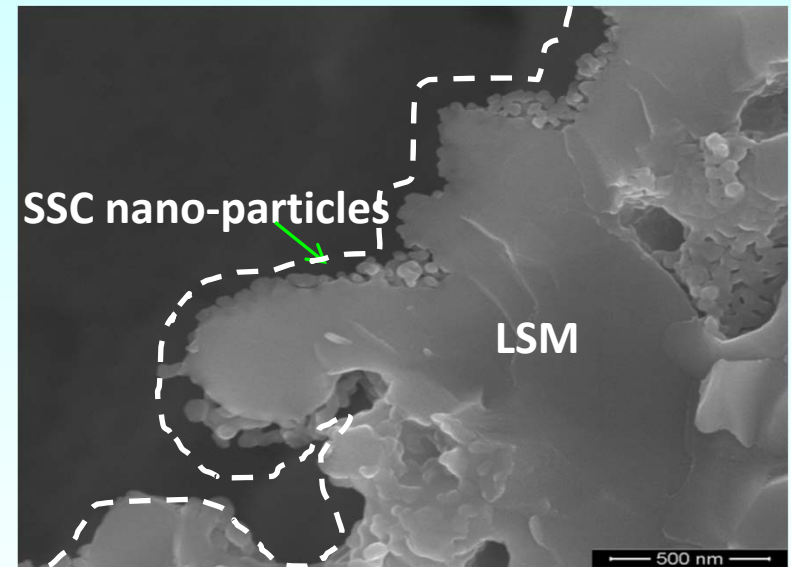
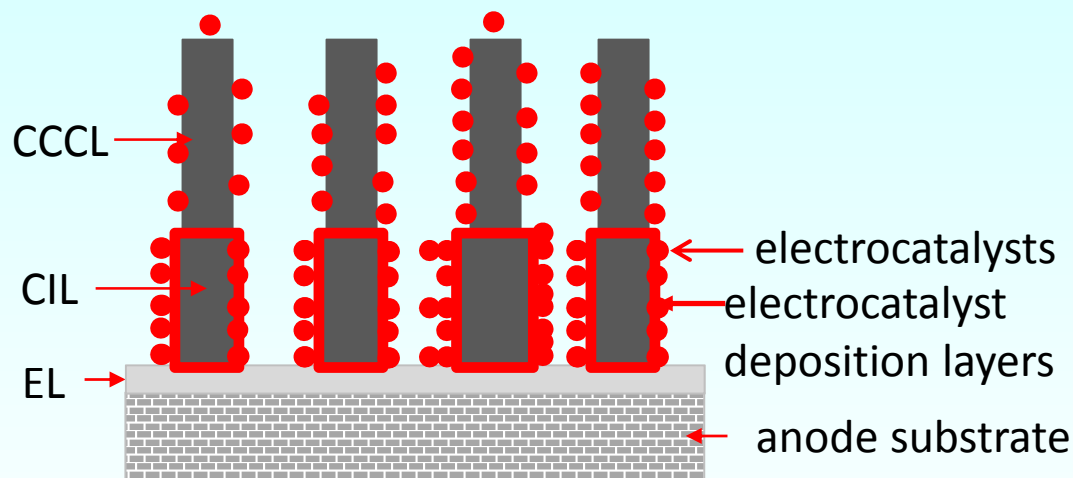


Diagram of the single-step Vacuum-Pressure-Infiltration-Thermal Treatment (VPIT) technique, involving:

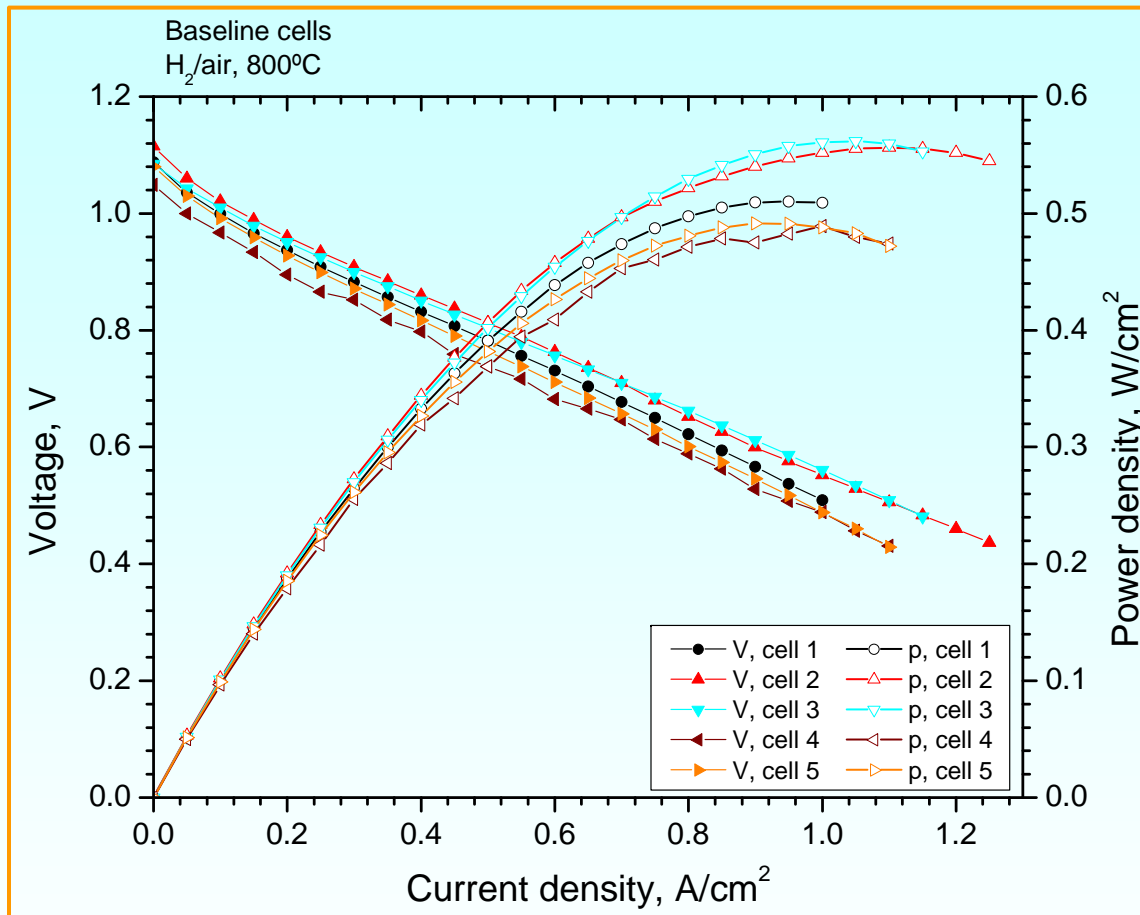
- Initial vacuum step to remove air entrapped inside the cathode backbones
- precipitation of a nitrate solution into the porous cathode backbones
- and immediately followed pressurization
- gelation/decomposition at a proper rate/temperature
- Calcination at elevated $T \sim 850^{\circ}\text{C}$
 - Evaluate effects of various electrocatalysts on performance improvement, e.g. SSC, LSC, LSM, LSCF
 - Repeatability/durability
 - Scaling up from 1"-button to 4"x4"

Infiltration Technique Implementation



- Reconstruct CIL and CTL to ensure an efficient infiltration of a catalyst quickly to the ERS (TPB & 2PB)
- Avoid excessive agglomerates and to ensure a good coverage of a catalyst along the cathode grains

Baseline Cell (LSM-based) Tests

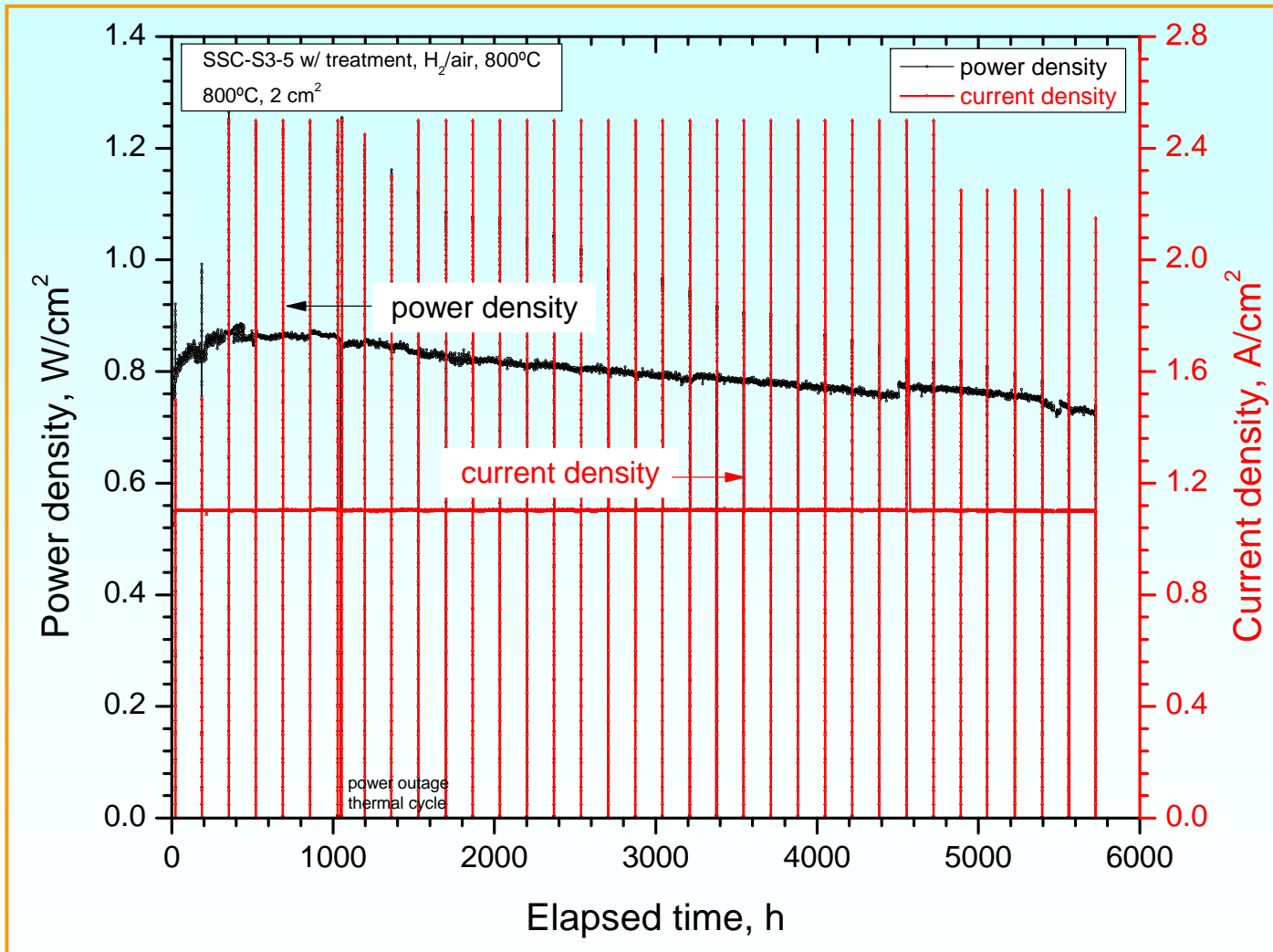


- Button cell baseline tests (w/o catalyst infiltration) for repeatability
- Typical power density: 0.4~0.5 W/cm² @ 0.7V; 0.5~0.56 W/cm² at peak

Baseline cell No.	Peak power density W/cm ²	Power density at 0.7V W/cm ²	ASR Ωcm ²
Cell No. 1	0.51	0.45	0.53
Cell No. 2	0.557	0.5	0.506
Cell No. 3	0.562	0.502	0.487
Cell No. 4	0.489	0.4	0.515
Cell No. 5	0.492	0.43	0.548

Nano Electrocatalyst Infiltration Effects

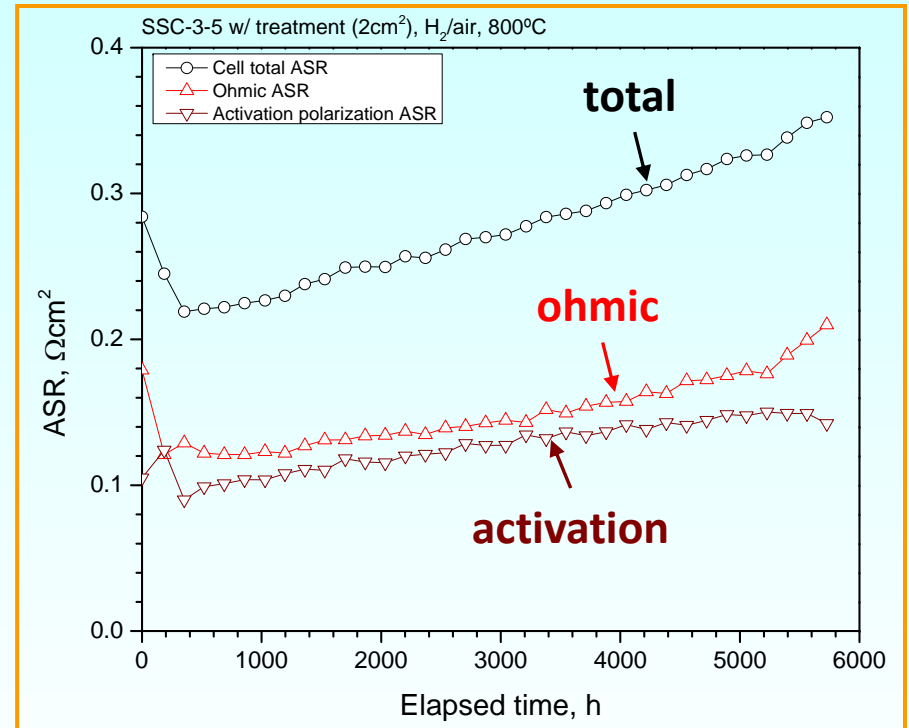
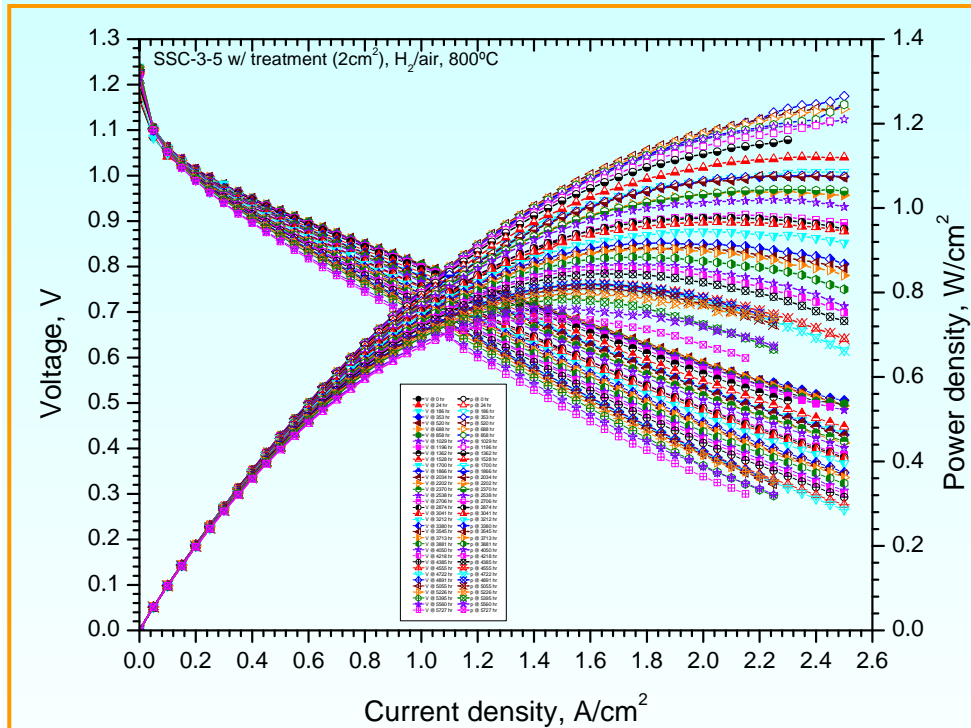
Long-term test results of a button cell



- 1" button cell (2cm²)
- T_{cell} @ 800C, H₂/air
- upon infiltration, cell power density at 0.7V increased from 0.55 W/cm² to 0.86 W/cm² (> **60% improvement**)
- performance improved over **+4.5%/1khrs** during the initial 1000 hrs test until a power outage,
- cell overall degradation rate @ **-2.56%/1khrs** over **57,00 hrs (over 8 months)**

Significance of Catalyst Infiltration

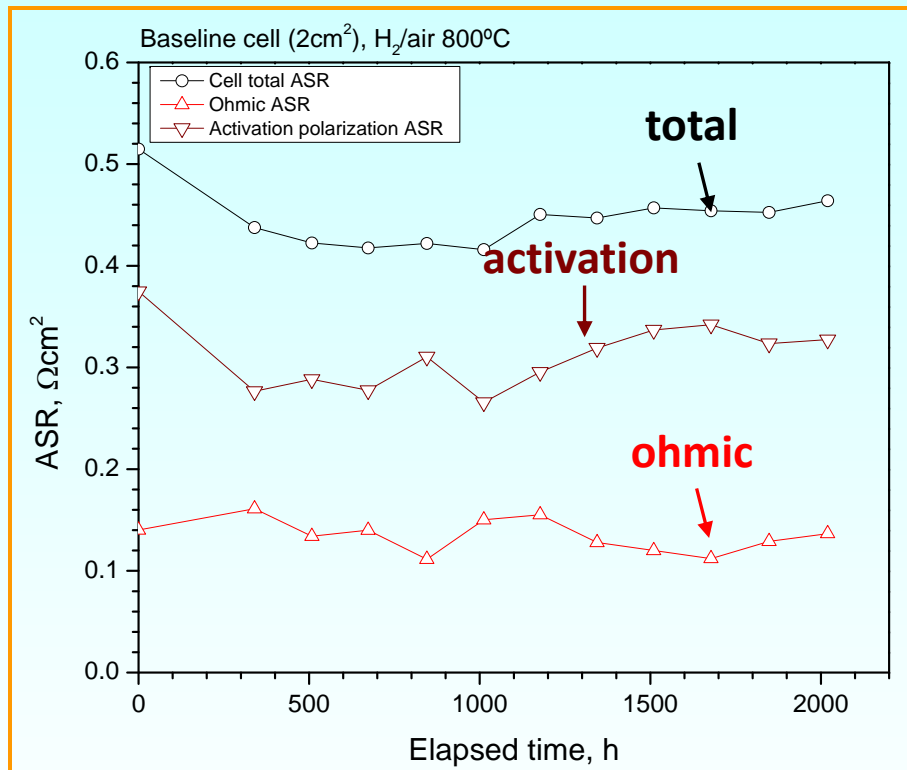
VI tests & EIS measurement at scheduled time (weekly)



Activation polarization losses were less than Ohmic losses

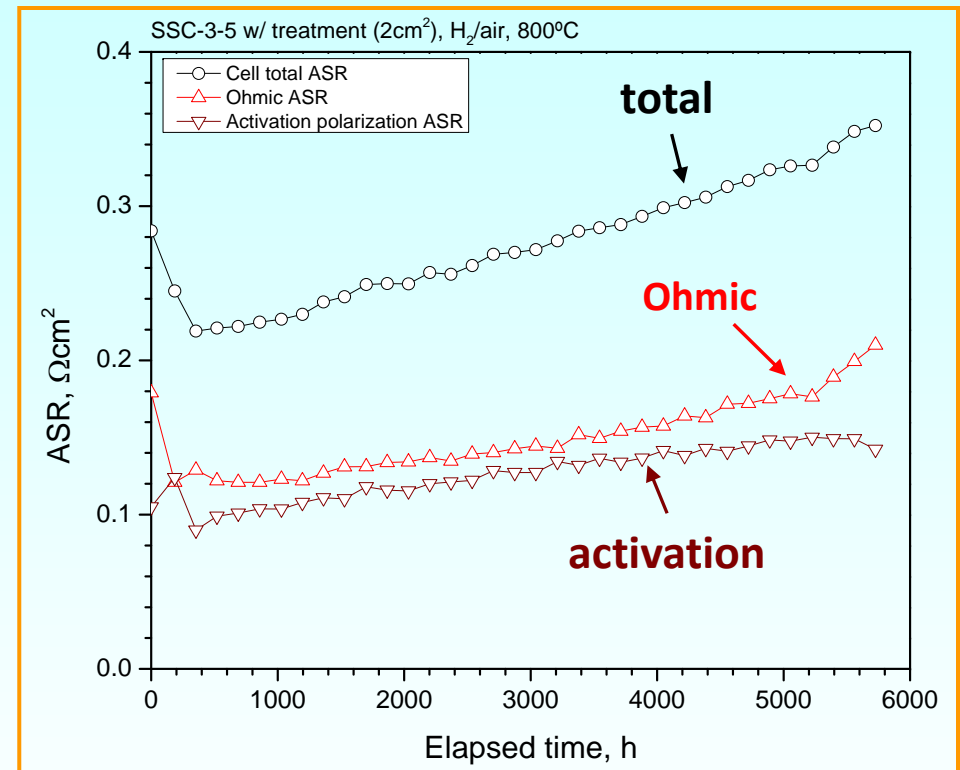
Benefits from Catalyst Infiltration – ASR standpoint

Baseline cell (w/o infiltration)



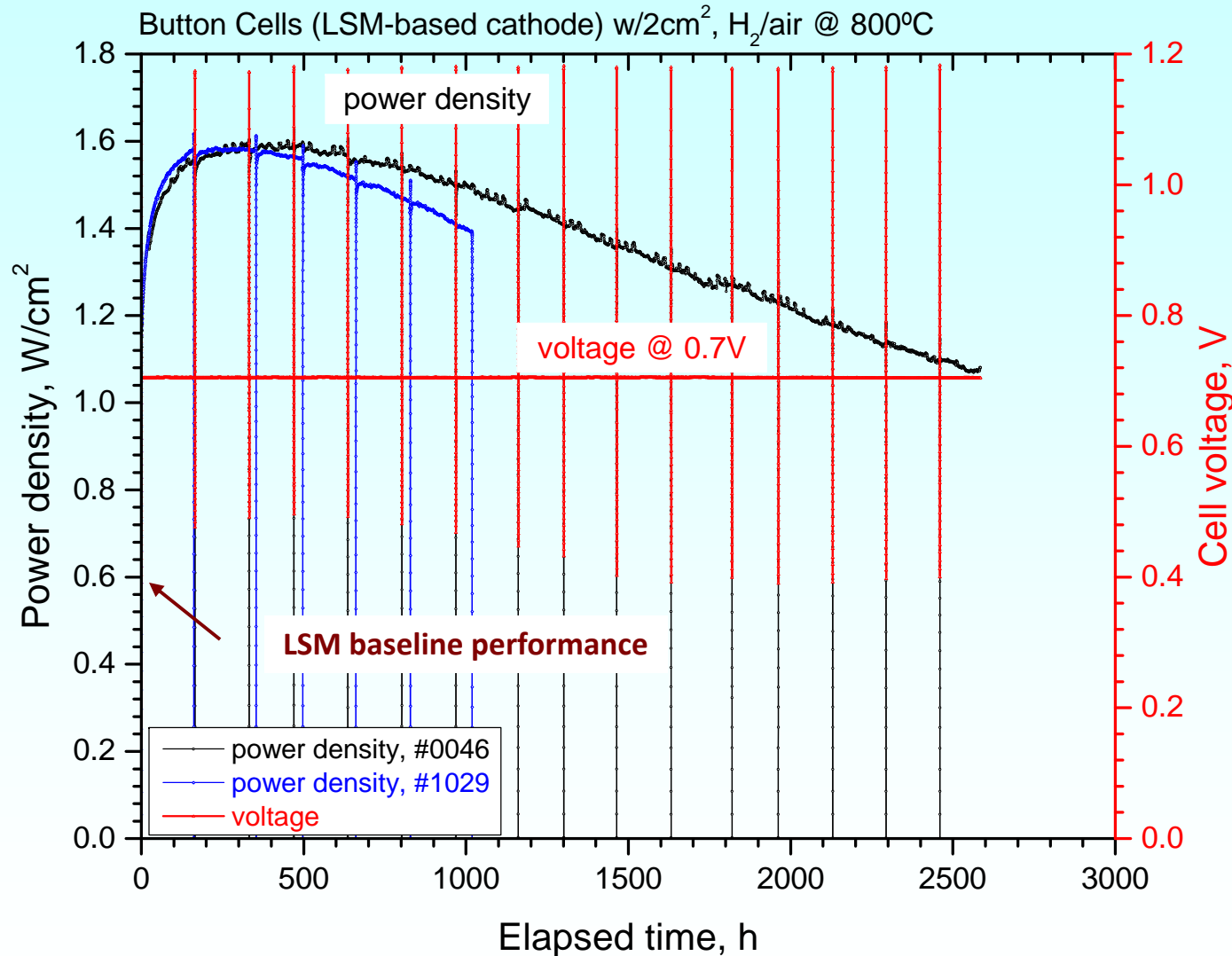
Cell ASR ~ 0.44 Ωcm² consisting of
 Ohmic ASR ~ 0.13 Ωcm²
 Activation ASR ~ 0.31 Ωcm²

Cell (infiltrated w/ SSC)



Cell ASR ~ 0.22 → 0.34 Ωcm² consisting of
 Ohmic ASR ~ 0.12 → 0.22 Ωcm²
 Activation ASR ~ 0.1 → 0.12 Ωcm²

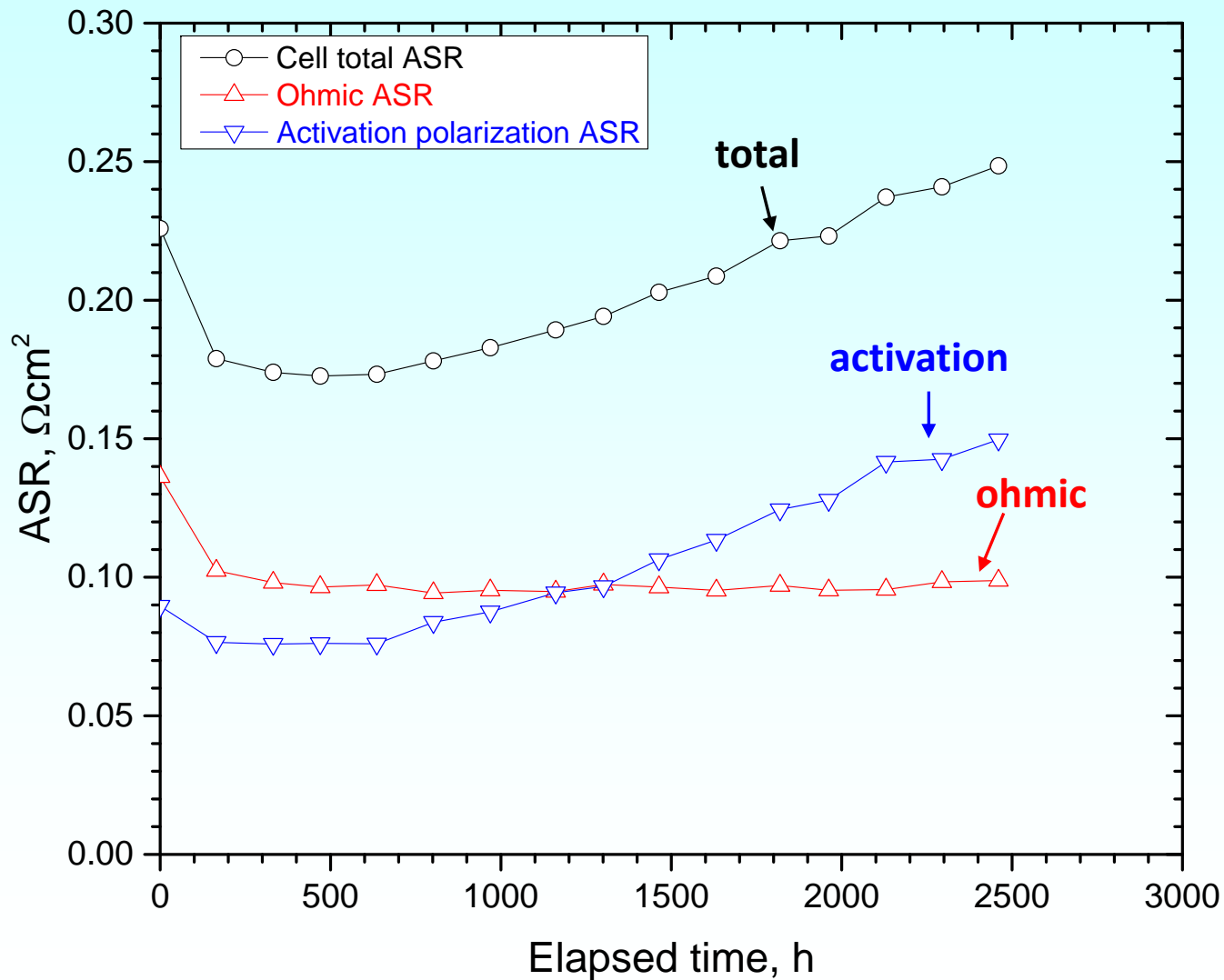
Nano-sized Super Electrocatalysts



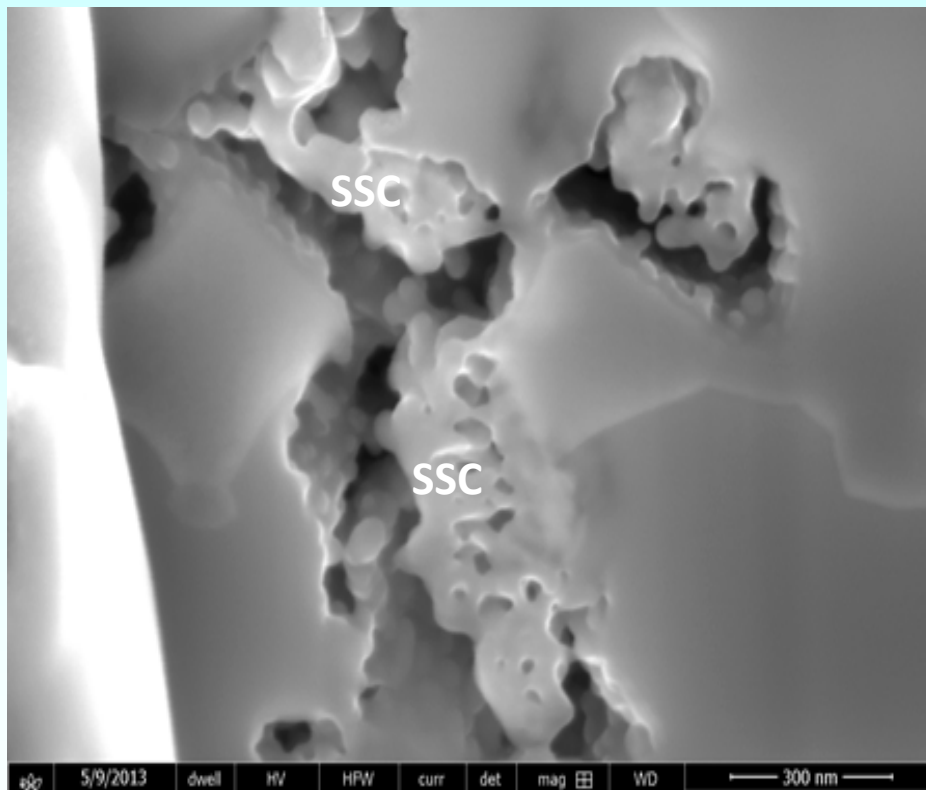
- Nano-sized electrocatalyst
- upon infiltration, cell p-density @ 0.7V increased from 0.55 W/cm² to **1.58 W/cm²** (> **180% improvement**)
- 1.5%/1khr improvement over 1khr test
- High degradation rate

Performance Characterization

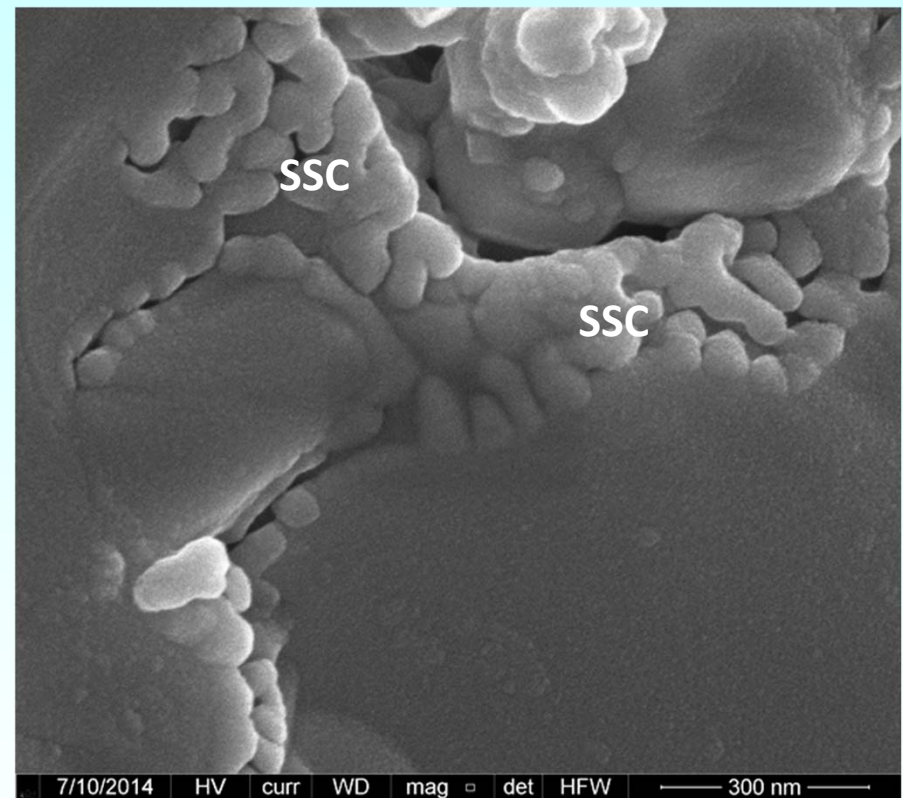
VI tests & EIS measurement at scheduled time (weekly)



Microstructure Changes after Long-term Tests

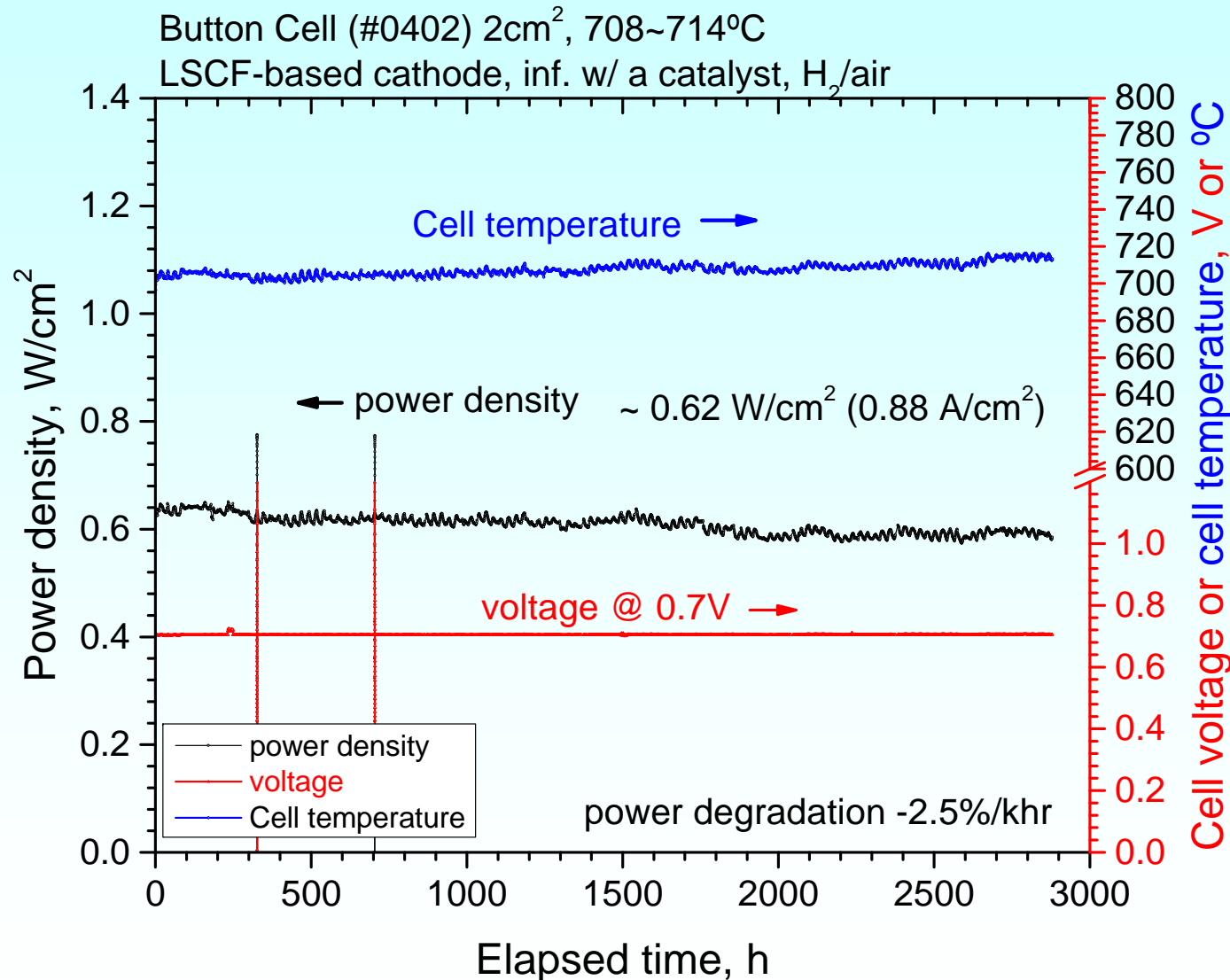


Pristine cell w/ SSC infiltration, sample was prepared by FIB cut near electrolyte (CIL)



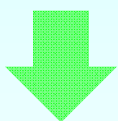
Cell after thousands of hours test.
Sample was prepared by FIB cut near electrolyte (CIL)

Electrocatalyst Effects on LSCF-base Cathode

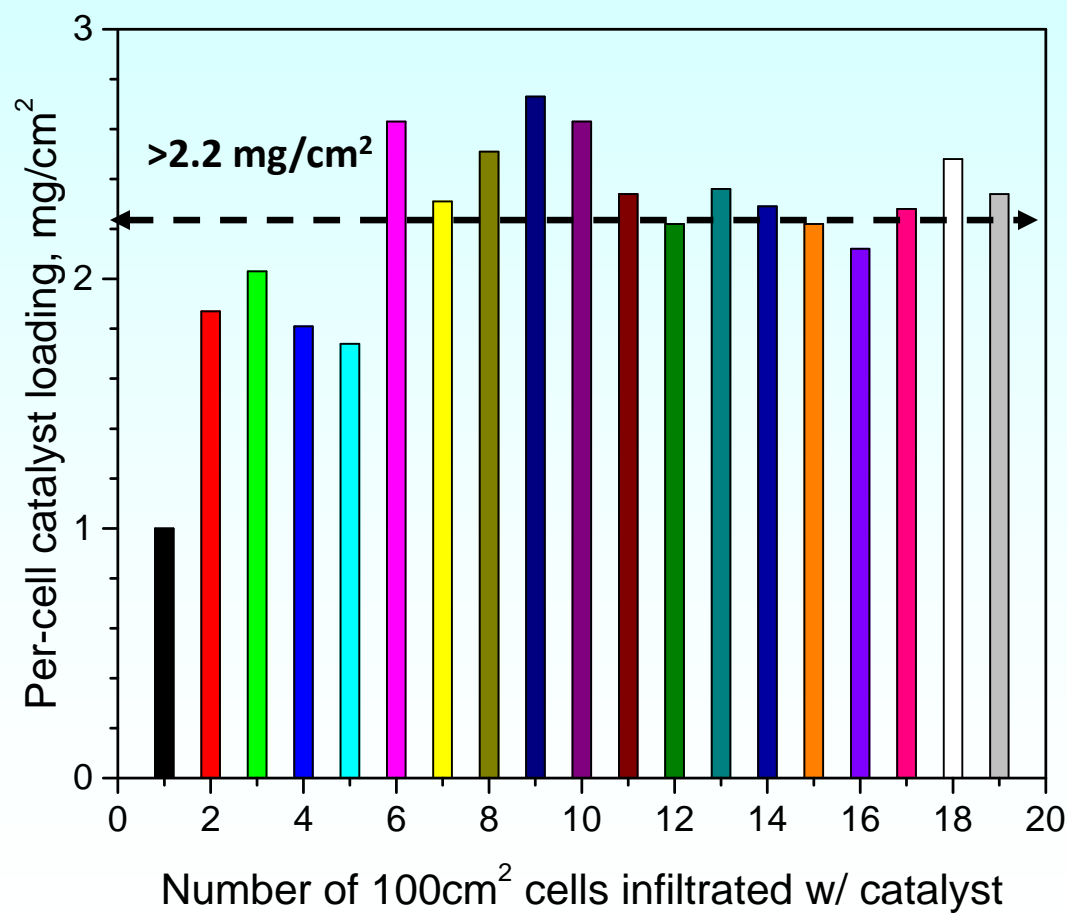


- LSCF-based cathode system experienced higher degradation @ high T
- A complex system compared to LSM-based
- Lowering operating T improves stability
- Fixed V@0.7V. (j @ ~ 0.88 A/cm²)
- Over 35% improvement upon electrocatalyst infiltration
- Power degradation rate ~ -2.5%/khr

From Button Cells to 100cm² Cells

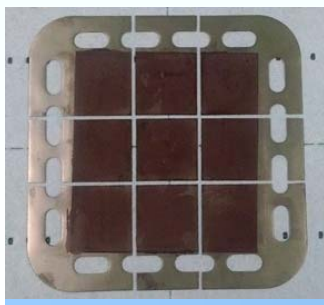
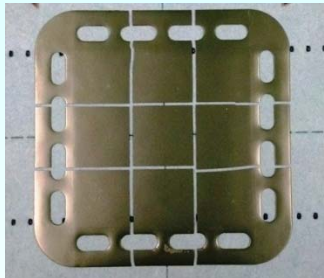


- Implement the infiltration technique to large cells
 - Scalability
 - Nano electrocatalyst distribution
 - Repeatability

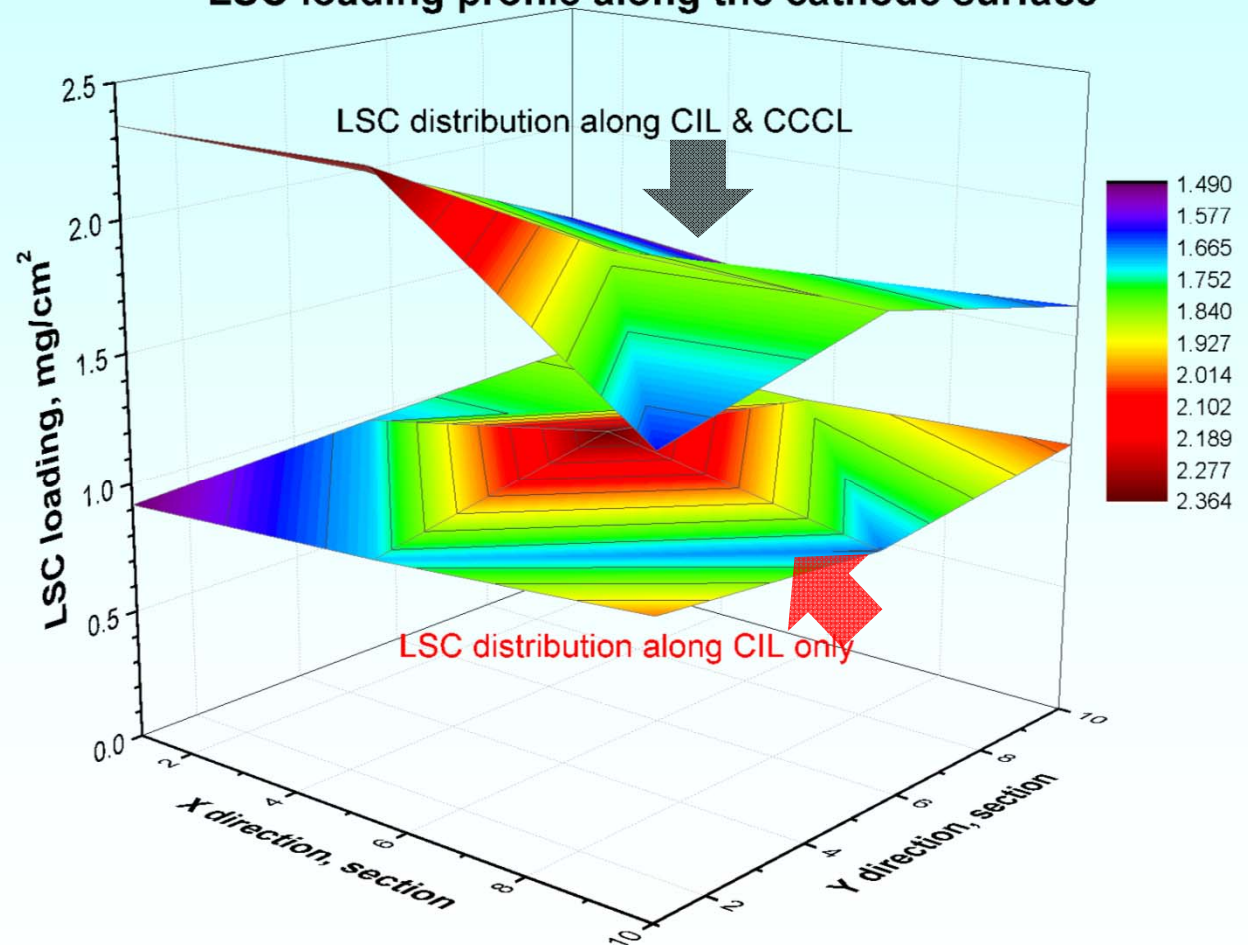


Catalyst Loading Profile Study

Study of LSC loading distribution along 4"x4" single cells (100 cm²) – characterization from corner to corner



LSC loading profile along the cathode surface

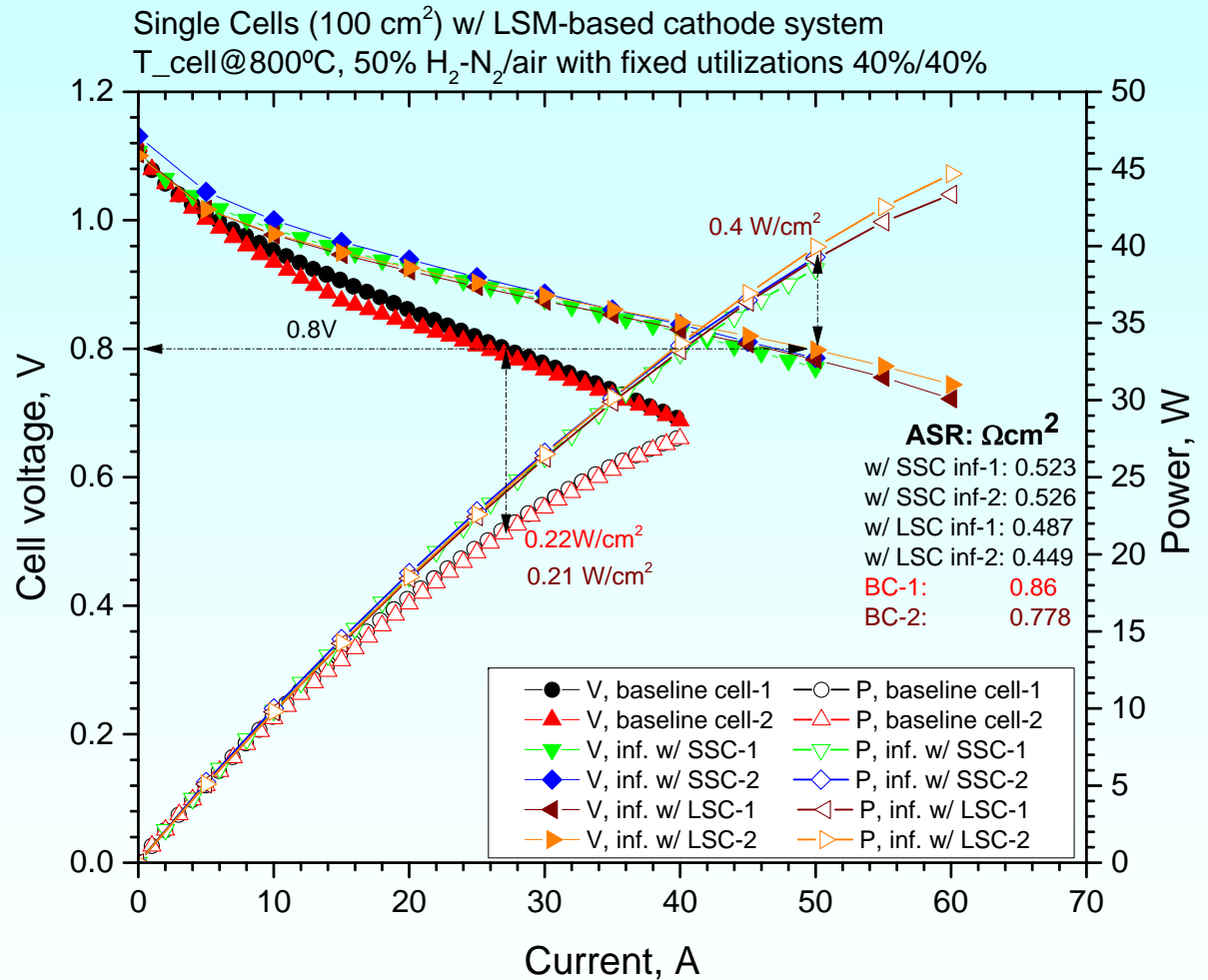


Single Cell (100 cm²) Evaluation



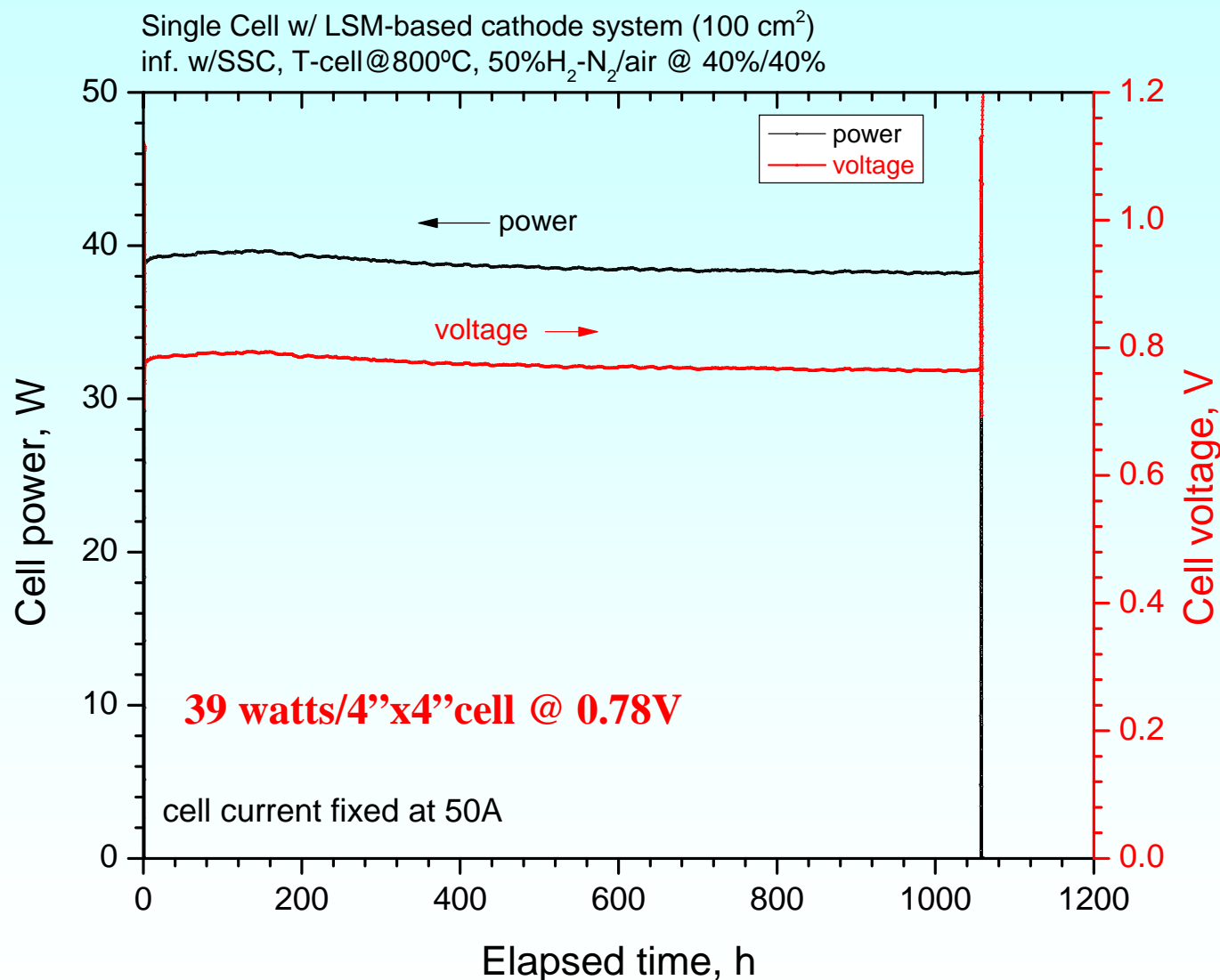
all-ceramic test-rig for single cell tests

- free-of Cr sources, but Cr-source can be introduced in a controlled fashion
- no metallic IC
- mimic stack compression & flow patterns
- Moisture can be introduced to both electrodes
- Flexible fuel feeds



Six-single cell performance comparison:
 two baseline cells, two w/ SSC inf. & 2 w/ LSC inf.

Long-term Test of a Single Cell w/ SSC Infiltration

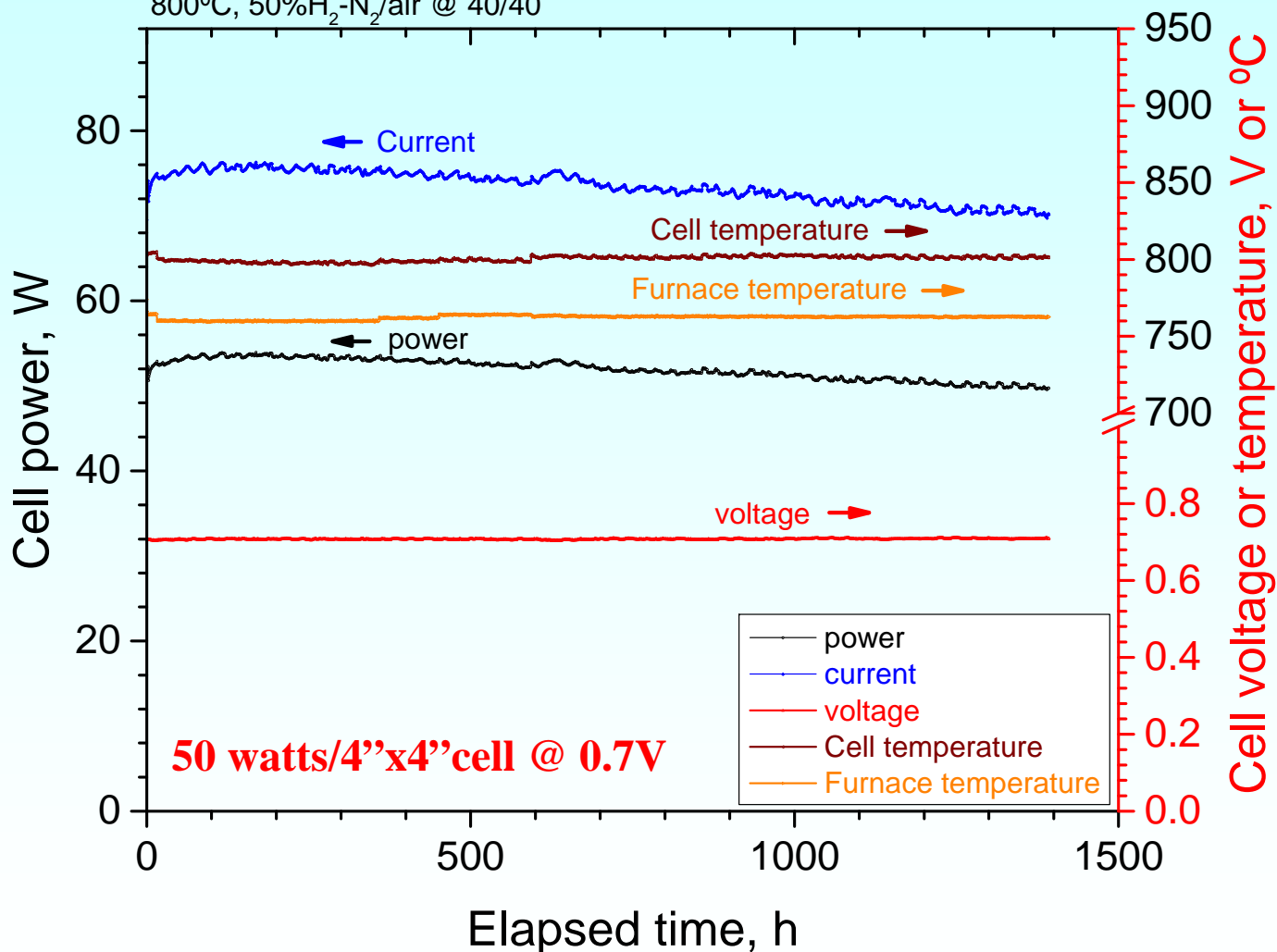


- ❖ Cell temperature adjusted to 800°C
- ❖ Dilute fuel w/ fixed 40% utilizations
- ❖ Under a constant current of 50 A (0.5A/cm²)
- ❖ Cell voltage ~ 0.78 V
- ❖ Power improved by ~ +2%/1khr during initial 200-hr test
- ❖ Over the 1khr test, power degradation rate: -3.5%/1khr, or -0.014 mW/cm²-hr

Long-term test result of a single cell w/ SSC infiltration

Long-term Test of a Single Cell w/ LSC Infiltration

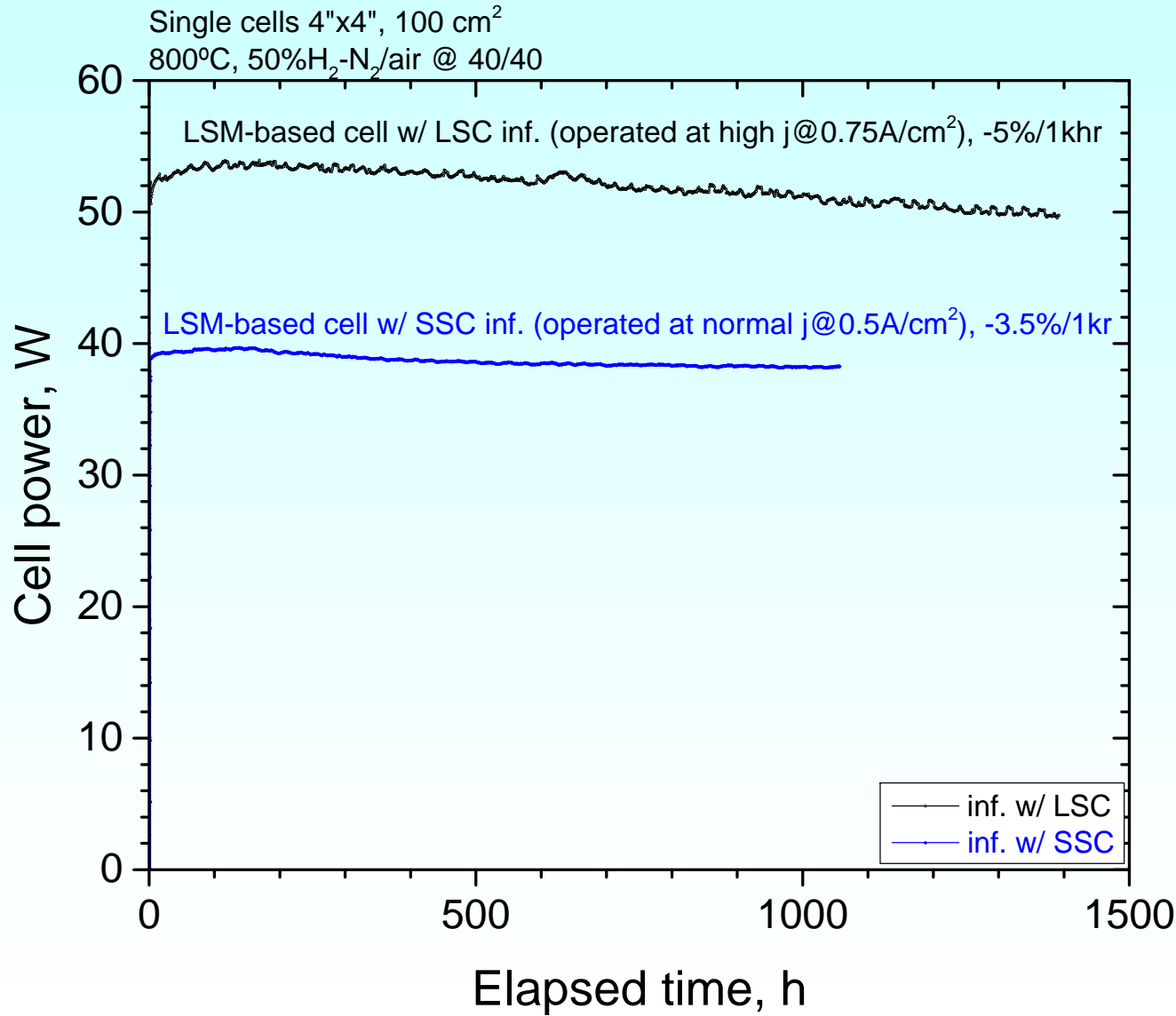
Single cell, fixed @ 0.7V
 LSM-LSC-2 #avi-a01 (batch 121109), 100 cm²
 800°C, 50%H₂-N₂/air @ 40/40



Long-term test result of a single cell w/ LSC infiltration

- ❖ TC to monitor cell cathode T (800°C)
- ❖ Furnace T was 760°C
- ❖ Dilute H₂ fuel w/ fixed 40% utilizations
- ❖ Under a C.V.@0.7V
- ❖ Cell current 75~71A (0.75~0.71 A/cm²)
- ❖ Power improved by ~ +12%/1khr during initial 200-hr test
- ❖ > 14,00-hr test (on-going), p degradation rate: -5%/1khr, or - 0.028 mW/cm²-hr

Cell Operating Condition Effect on Degradation

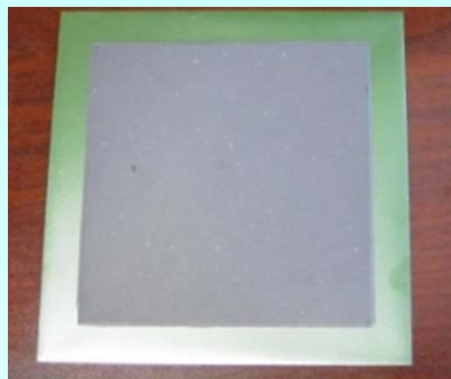


- ❖ Effects of cell operating conditions on cell life
- ❖ Higher performance had higher degradation rate
- ❖ “sweet spot” operating conditions? (need “Hurricane Model” for prediction)

Scale-up Ability



2.8 W/cell (1.4W/cm²)

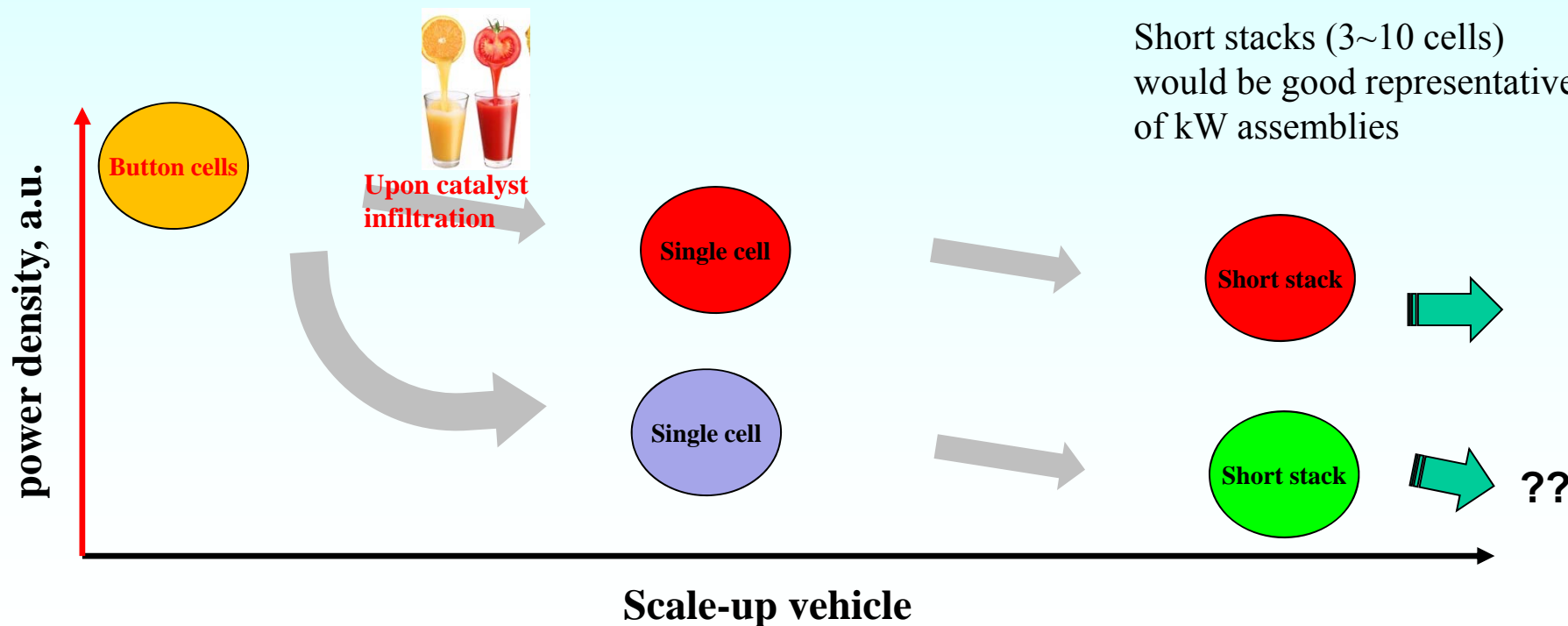


50 W/cell (0.5 W/cm²)

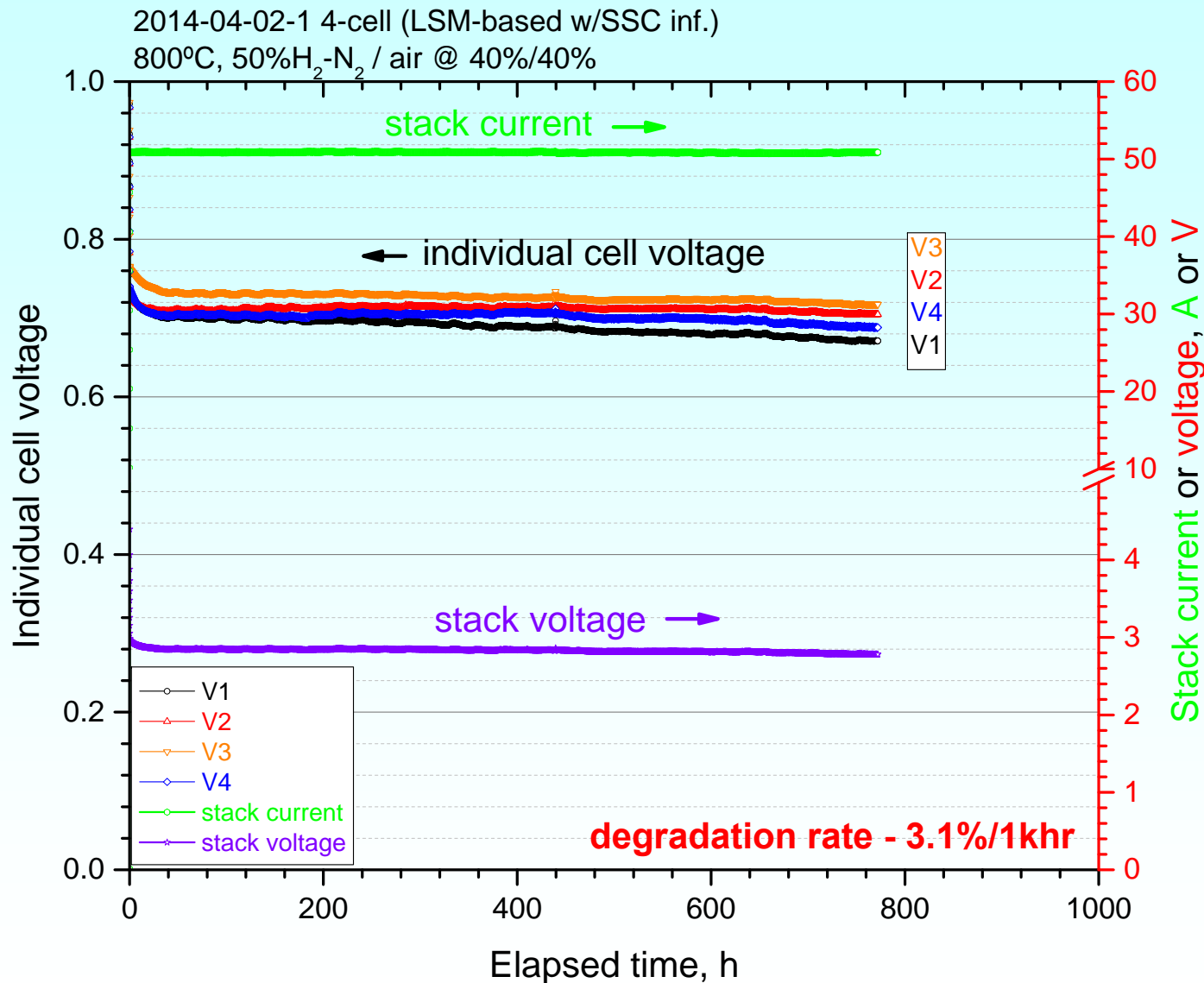


145 W/4-cell stack (0.36 W/cm²)

Short stacks (3~10 cells) would be good representative of kW assemblies



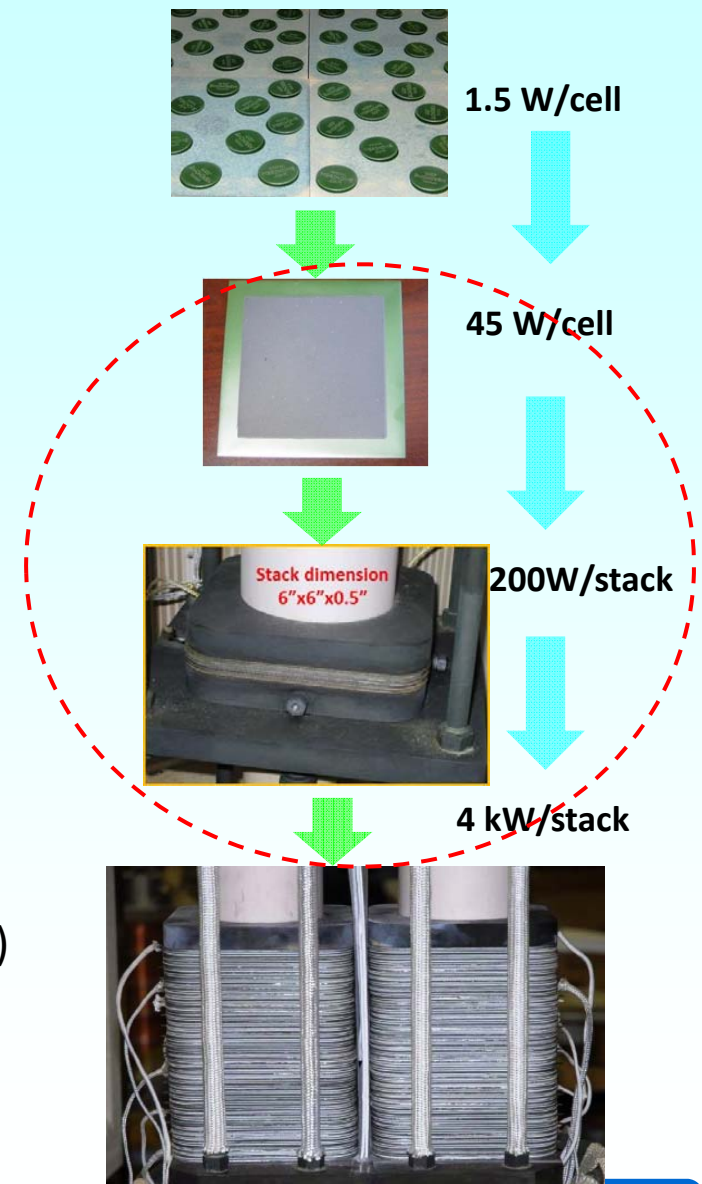
Short Stack Validation



- ❖ All four cells were infiltrated w/ SSC
- ❖ Top/bottom cell had relatively lower performance than middle cells
- ❖ Overall stack performance improvement > 30% after infiltration
- ❖ Degradation rate ~ -3.1%/1khr

Summary/Future Work

- Infiltration of a nano-sized electrocatalyst can be an efficient and cost-effective approach to improve SOFC cathode performance;
- Key parameters determining the single-step infiltration efficiency are critical to the success of the SOFC performance improvement. However, certain protocols have to be developed for implementing infiltration process on scalable cells;
- Continue to perfect the VPIT processes
 - Explore other catalyst effects under various operating conditions
 - Optimize catalyst structure
 - Identify the electrode degradation attributions
 - Perform techno-economic evaluation
- Evaluate scale-up cells (100 cm²) and stacks (200W class) for proof-of-concept demonstration (built-on MSRI's standard SOFC products/ platforms)



Acknowledgement

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- Phase II Project Manager Joseph Stoffa, Briggs White, Shailesh Vora, and the entire NETL SECA program management team

Thank you!

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